



First Order Derivatives of Thermodynamic Functions under Assumption of no Chemical Changes



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DIFFERENTIALS

The total differential of a function f of several variables is the sum of all partial differentials [1]. In the absence of chemical changes, all state thermodynamic parameters are total differentials and depend on two variables (Table 1).

Table 1. Differentials of thermodynamic parameters

| | |
|---|-------------------------------------|
| $dE = T \cdot dS - p \cdot dV + \sum_i \mu_i \cdot dn_i$ | in the presence of chemical changes |
| $dn_i = 0$ for each i | provided that no chemical changes |
| $dE = T \cdot dS - p \cdot dV$ | in the absence of chemical changes |
| E = internal energy; S = entropy; V = volume; n = number of particles | |

[1] M. Hazewinkel, Encyclopaedia of Mathematics: An Updated and Annotated Translation of the Soviet "Mathematical Encyclopaedia." Dordrecht, Netherlands: Reidel, 1988, p. 228.

OBJECTIVES

- Identifying the heat from reversible process $dQ_{\text{rev}} = T \cdot dS$ and mechanical work in the form of that from quasi-static processes $dw_{\text{cvs}} = -p \cdot dV$, these two thermodynamic quantities (dQ and dw) became total differentials. The condensed collection of the Bridgman's thermodynamic equations [2] was used as starting point in this study. A series of codification schemas were developed and implemented in order to obtain all first order partial derivatives [3] (Table 2).

[2] P.W. Bridgman, A complete collection of thermodynamic formulas, Phys. Rev. 3, 1914, 273-281.

[3] L. Jäntschi, General Chemistry Course, AcademicDirect Publishing House, 2013.

BRIDGMAN'S THERMODYNAMIC EQUATIONS

Table 2. Gradients after pressure (p), volume (V) and temperature (T) of an unknown function (f)

| Variable | | | $\left. \frac{\partial f}{\partial x} \right _{z=ct} = \left. \frac{\partial f}{\partial x} \right _{y=ct} + \left. \frac{\partial f}{\partial y} \right _{x=ct} \cdot \left. \frac{\partial y}{\partial x} \right _{z=ct}$ | $\left. \frac{\partial f}{\partial z} \right _{x=ct} = \left. \frac{\partial f}{\partial y} \right _{x=ct} \cdot \left. \frac{\partial y}{\partial z} \right _{x=ct}$ | Order |
|----------|---|---|---|---|---------|
| z | x | y | $f_{xz} = f_{xy} + f_{yx} \cdot y_{xz}$ | $f_{zx} = f_{yx} \cdot y_{zx}$ | $f = E$ |
| p | T | V | $f_{pV} = f_{pT} + f_{Tp} \cdot T_{pV}$ | $f_{Vp} = f_{Tp} \cdot T_{Vp}$ | 6 |
| p | V | T | $f_{pT} = f_{pV} + f_{Vp} \cdot V_{pT}$ | $f_{Tp} = f_{Vp} \cdot V_{Tp}$ | 5 |
| T | p | V | $f_{TV} = f_{Tp} + f_{pT} \cdot p_{TV}$ | $f_{VT} = f_{pT} \cdot p_{VT}$ | 2 |
| T | V | p | $f_{Tp} = f_{TV} + f_{VT} \cdot V_{Tp}$ | $f_{pT} = f_{VT} \cdot V_{pT}$ | 4 |
| V | p | T | $f_{VT} = f_{Vp} + f_{pV} \cdot p_{VT}$ | $f_{TV} = f_{pV} \cdot p_{TV}$ | 1 |
| V | T | p | $f_{Vp} = f_{VT} + f_{TV} \cdot T_{Vp}$ | $f_{pV} = f_{TV} \cdot T_{pV}$ | 3 |

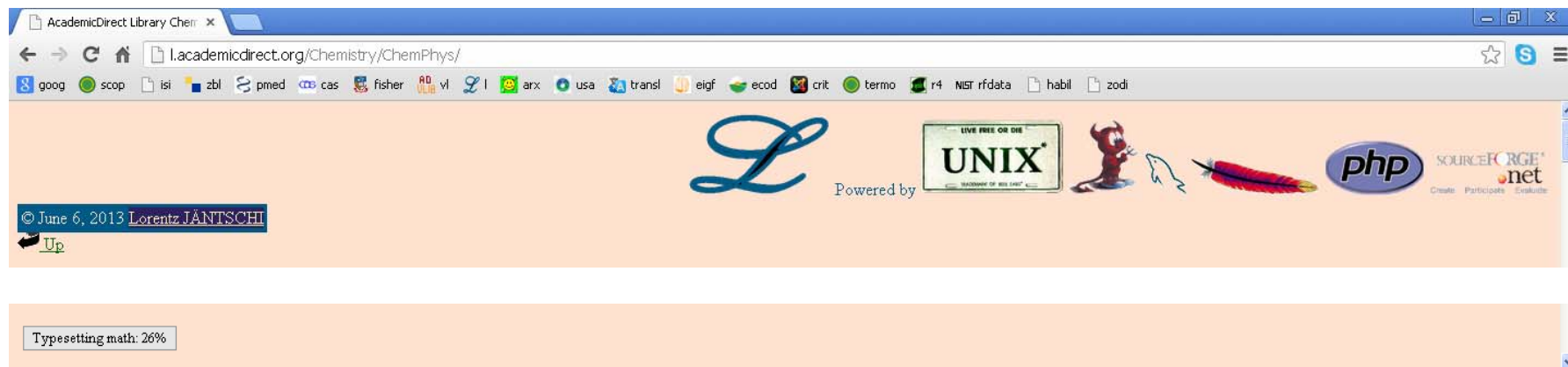
RESULTS

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- Inputs: state parameters, process differentials, thermodynamic equations and gradients.
- Output: first order partial derivatives, counting a number of two-hundred and forty equations
- <http://l.academicdirect.org/Chemistry/ChemPhys/>

RESULTS

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Typesetting math: 26%

Equations: 240

RESULTS

| State parameters | | | Process differentials | | |
|------------------|--|--------------------------------|---|--|------------------|
| Type | Parameter | Meaning | Type | Parameter | Meaning |
| Intensive | P | Pressure | Extensive | dQ | Heat |
| Intensive | T | Temperature | Extensive | dw | Work |
| Extensive | V | Volume | Extensive | $dQ_r \stackrel{\text{def}}{=} T \cdot dS$ | Reversible heat |
| Extensive | S | Entropy | Extensive | $dw_c \stackrel{\text{def}}{=} -p \cdot dV$ | Quasistatic work |
| Extensive | E | Internal energy | Consequence | | |
| Extensive | N | Number of particles | A reversible process is quasistatic | | |
| Extensive | $H \stackrel{\text{def}}{=} E + pV$ | Enthalpy | Equations | | |
| Extensive | $A \stackrel{\text{def}}{=} E - TS$ | Helmholtz energy | Equation | Comments | |
| Extensive | $G \stackrel{\text{def}}{=} E + pV - TS$ | Gibbs energy | $dE = dQ + dw$ | for a system with no chemical changes | |
| Exact | N_A | Avogadro's number of particles | $dE = dQ + dw + \sum_i \mu_{N,i} dN_i$ | general law ($\mu_i \stackrel{\text{def}}{=} N_A \mu_{N,i}$) | |
| Extensive | $n \stackrel{\text{def}}{=} \frac{N}{N_A}$ | Amount of substance (mols) | $dE = dQ + dw + \sum_i \mu_i dn_i$ | Integral general law (assumes null integration constant) | |
| Intensive | $V_m \stackrel{\text{def}}{=} \frac{V}{n}$ | Molar volume | $E = Q + w + \sum_i \int \mu_i dn_i$ | | |
| Intensive | $S_m \stackrel{\text{def}}{=} \frac{S}{n}$ | Molar entropy | $dE = dQ - pdV + \sum_i \mu_i dn_i$ | quasistatic | |
| Intensive | $E_m \stackrel{\text{def}}{=} \frac{E}{n}$ | Molar internal energy | $dH = dQ + Vdp + \sum_i \mu_i dn_i$ | (dw = -pdV) | |
| Intensive | $H_m \stackrel{\text{def}}{=} \frac{H}{n}$ | Molar enthalpy | $dA = dQ - pdV - TdS - SdT + \sum_i \mu_i dn_i$ | processes | |
| Intensive | $A_m \stackrel{\text{def}}{=} \frac{A}{n}$ | Molar Helmholtz energy | $dG = dQ + Vdp - TdS - SdT + \sum_i \mu_i dn_i$ | | |
| Intensive | $G_m \stackrel{\text{def}}{=} \frac{G}{n}$ | Molar Gibbs energy | $dE = TdS - pdV + \sum_i \mu_i dn_i$ | reversible (dQ = TdS) | |
| Intensive | $J \stackrel{\text{def}}{=} \frac{2E}{pV}$ | Number of energy components | $dH = TdS + Vdp + \sum_i \mu_i dn_i$ | & | |
| | | | $dA = -pdV - SdT + \sum_i \mu_i dn_i$ | quasistatic (dw = -pdV) | |
| | | | $dG = Vdp - SdT + \sum_i \mu_i dn_i$ | processes | |

RESULTS

| Gradients | |
|---|--|
| Gradient | Formula |
| Isothermal compressibility | $\beta_T \stackrel{\text{def}}{=} -\frac{1}{V} \cdot \frac{\partial V}{\partial p} \Big _{T=\text{ct.}}$ |
| Volumetric coefficient of thermal expansion | $\alpha_V \stackrel{\text{def}}{=} \frac{1}{V} \cdot \frac{\partial V}{\partial T} \Big _{p=\text{ct.}}$ |
| Heat capacity at constant pressure | $C_p \stackrel{\text{def}}{=} \frac{\partial H}{\partial T} \Big _{p=\text{ct.}}$ |
| Joule-Thomson isothermal coefficient | $\mu_T \stackrel{\text{def}}{=} \frac{\partial H}{\partial p} \Big _{T=\text{ct.}}$ |
| Heat capacity at constant volume | $C_V \stackrel{\text{def}}{=} \frac{\partial E}{\partial T} \Big _{V=\text{ct.}}$ |
| Internal pressure | $\pi_T \stackrel{\text{def}}{=} \frac{\partial E}{\partial V} \Big _{T=\text{ct.}}$ |

To do: first and second partial derivatives

$$\frac{\partial E}{\partial G} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{S \cdot V + S \cdot p \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} + p \cdot V \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}$$

$$\frac{\partial E}{\partial H} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{S \cdot V + p \cdot V \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - S \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - p \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}}}$$

$$\frac{\partial E}{\partial Q} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - S \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}$$

$$\frac{\partial E}{\partial S} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{- \frac{p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}}}{T} - \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - S \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}$$

FUTHER WORK

- The transformation of an interactive interrogation is conducted in our lab in order to allow selecting the function, the variable and the constant before generation of the thermodynamic equation first order derivatives.

Thank you for your attention!

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